

**FEASIBILITY REPORT**

**(PROJECT FEASIBILITY REPORT)**

**O N**

**MAIZE AND ITS BYE PRODUCTS**



**IDENTIFICATION & EVALUATION DIVISION FOR HI-TECH PROJECTS**

**ENGINEERS INDIA RESEARCH INSTITUTE**

**EIRI CONSULTANTS & ENGINEERS**

**\* REGD. OFFICE \***  
4449, NAI SARAK, MAIN ROAD,  
NEAR CHANDNI CHOWK,  
DELHI - 11 00 06. (INDIA)  
(BETWEEN MARWARI KATRA AND ROSHAN PURA),  
PH : 91-11-23918117, 23916431, 45120361, 64727385, 23947058  
E-Mail : eiriprojects@gmail.com, eiribooks@yahoo.com  
Web: www.eiriindia.org, www.eiribooksandprojectreports.com

CODE : EIRI/DFR/7305  
J.C. : 9941

## C A U T I O N

This project report has been prepared on the basis of information available with **M/S. ENGINEERS INDIA RESEARCH INSTITUTE**. The intention here is to provide preliminary information to the prospective entrepreneur. Prior to making a firm decision for investment in the project the entrepreneur must verify the various feasibility aspects together along with the addresses for the procurement of plant & machinery and raw materials independently. The information supplied in this report is obtained from the reliable sources but it is not guaranteed and the money once paid will not be refunded back in any case. Claims for incomprehensiveness of the project report will not be entertained and no legal action in this regard would be entertained in any case (Subject to Delhi Jurisdiction only). Any matter relating to our standard points covered in the report may be modified with in 5 days time only from the date of purchase.

**ENGINEERS INDIA RESEARCH INSTITUTE, 4449 NAI SARA, DELHI-110006.**

## **MAIZE AND ITS BYE PRODUCTS**

**[EIRI/DFR/7305] J.C.:9941**

### **CONTENTS**

#### **APPENDIX -A**

01. PLANT ECONOMICS	A-1
02. LAND & BUILDING	A-2
03. PLANT AND MACHINERY	A-3
04. OTHER FIXED ASSESTS	A-4
05. FIXED CAPITAL	A-5
06. RAW MATERIAL	A-6
07. SALARY AND WAGES	A-7
08. UTILITIES AND OVERHEADS	A-8
09. TOTAL WORKING CAPITAL	A-9
10. TOTAL CAPITAL INVESTMENT	A-10
11. COST OF PRODUCTION	A-11
12. TURN OVER/ANNUM	A-12
13. BREAK EVEN POINT	A-13
14. RESOURCES FOR FINANCE	A-14

# **MAIZE AND ITS BYE PRODUCTS**

**[EIRI/DFR/7305] J.C.:9941**

## **INTRODUCTION**

### **Starch Industry in India**

Starch is an abundant carbohydrate distributed worldwide in plants. Starch has been a major ingredient in man's diet over the centuries. In addition it has become a major industrial raw material. Plant seeds, roots and tubers are all sources of industrial starch production. The commercial realities of the starch recovery process limit the industrial sources mainly to wheat, maize and tapioca. Indian starch industry mainly consumes maize as input raw material.

Also some industries are tapioca based.

Maize is doing wonderful things in our everyday life. Maize is present in one form or other in

The Food we eat

The Milk we drink

The Chocolates/Biscuits we take

The Clothes we wear

The Paper we read

The Medicines we take

Maize (Corn) contains about 70% starch, other components being protein, fibers and fat. The basis of the maize milling process is the separation of the maize kernel into its different parts. Maize starch is produced by the wet milling process, which involves grinding of softened maize and separation of corn oil seeds (germs), gluten (proteins), fibers (husk) and finally pure starch.

## **Byproducts from Maize**

The byproducts from maize based industries find various applications:

- i. **Maize(Corn) Steep Liquor** : It contains amino acids, proteins and are used by antibiotics drugs manufacturers. Also it is a large source of biogas, which is being used as fuel for driers, boilers etc.
- ii. **Maize Gum** : Corn Oil is produced by expelling oil from the germs. Corn Oil finds applications in food and other chemical industries. Maize oil cake obtained after expelling oil is used as cattle and poultry feeds.
- iii. **Maize Gluten** : Maize Gluten contains high protein content and it is used as cattle and poultry feeds.
- iv. **Maize Husk** : It contains starch, protein and fat as minor components and mainly consumed as cattle feed.

## **1.0 Starches**

Starch is a group of polysacchrides, composed of glucopyranose units joined together by-glucosidric linkages. It conforms to the molecular formula,  $(C_6H_{10}O_5)_n$ , where  $n$  varies from a few hundred to over one million. Starch is found as the reserve carbonhydrate in various parts of plants and is enzymatically broken down to glucose to other carbohydrates according to the metabolic needs of the plants.

Industrially, starch is broadly divided into two types viz, natural and modified. Natural starches, also designated as unmodified starches or simply starches, are obtained from grains such as wheat and sorghum. from roots like potato, tapioca and arrow root, and from the pith of the stems of certain palms such as sago. They are further classified into cereal starches and root starches. The characteristics of the natural starches are changed by chemical or enzymatic action and the products of these reactions are termed modified starches. This group includes dextrans, acid-modified starches, oxidized starches, starch esters, starch ethers, dialdehyde starches, and cationic starches.

## **1.1 Natural Starches**

Starch occurs naturally in the plants and its percentage varies with the plant and also in different parts of the same plant. Corn (maize) sorghum grain wheat, rice, potato, tapioca, arrowroot and sago are among the important sources of natural starches. The grains of barley, rye, oat, and the millets are also employed in the production of starches.

## **1.1 Natural Starches**

Starch occurs naturally in the plants and its percentage varies with the plant and also in different parts of the same plant. Corn (maize) sorghum grain wheat, rice, potato, tapioca, arrowroot and sago are among the important sources of natural starches. The grains of barley, rye, oat and the illets are also employed in the production of starches.

## **1.2 Tapioca**

The roots of tapioca plant (*manihot utilissima*) forms one of the major sources of starch, ranking next to potato in the consumption by starch industry. Tapioca plant, also known as cassava and manioc, thrives in equatorial regions between the Tropic of Capricorn. There are as many as seventy five varieties of cassava plant of which two varieties viz., bitter and sweet are widely cultivated; the bitter is usually grown for the purposes of the manufacture of starch, as it contains a higher content of starch. The starch content of the plant varies between 12 and 33 per cent. The ratio of the percentage of amylose to amylopectin has been found to be 16:84. More than half of the total world acreage under the cultivation of cassava is confined to the African countries such as Gambia, Ghana, Kenya, Mauritius, Nigeria, Zambia, Nyassaland, Sierra Leone and Zanzibar and the rest come from the tropical regions of other continents.

### **1.3 Cereal Starches**

The cereal starches, such as maize, wheat, rice and sorghum, are recovered by several processes, of which the wet-milling is by far the most important. Other processes commercially employed in the manufacture of unmodified starches are that alkali, Martin and batter in the order of decreasing importance. Of the material methods earlier used for the production of starch and which have now become obsolete, mention may be made of the Hakka, Alsation and Fescas processes. In all the above processes, Starch is recovered in five stages:

- a) Softening or steeping of the grains, after thorough washing in water.
- b) Tabling or centrifugation of the ground mass.
- c) Dewatering and drying of the final products.
- d) The recovery of important by products.

### **1.4 Raw Materials**

The principal raw materials, used by the Indian Starch Industry are maize and tapioca.

#### **1.4.1 Maize**

Maize is grown in Uttar Pradesh, Bihar, Rajasthan, Punjab, Madhya Pradesh, Himachal Pradesh, Gujarat, Jammu and Kashmir, Andhra Pradesh, Mysore, and Haryana.

#### **1.4.2 Sorghum Grains**

Known as jowar in India, this material is widely cultivated in Mysore, Maharashtra, Madhya Pradesh, Andhra Pradesh, Rajasthan, Tamil Nadu, Gujarat, Uttar Pradesh, Orissa and Punjab.

### **1.4.3 Bajra**

Bajra is cultivated in Rajasthan, Gujarat, Uttar Pradesh, Haryana, Maharashtra, Tamil Nadu, Andhra Pradesh, Mysore, Punjab and Madhya Pradesh .

### **1.4.4 Small millets**

This group comprises French millets (*Panicum milliaceum*), little millets (*Panicum miliare*), Italian millet (*Setaria italica*) and other millets from *Echinochloa crus-galli*, *E.frumenaceum*, and *paspalum scrobiculatum*. Small millets are cultivated in an area of 4,732,00 hectares, distributed in the states of Madhya Pradesh, Tamil Nadu, Uttar Pradesh, Andhra Pradesh, Gujarat, Bihar, Mysore, Maharashtra, and Rajasthan.

### **1.4.5 Wheat**

It is one of the principal food grains of India. It is cultivated chiefly in Uttar Pradesh, Punjab, Gujarat, Maharashtra, Rajasthan, Bihar, Haryana, and Himachal Pradesh. respectively .

### **1.4.6 Chemicals**

The important chemicals used by the starch industry are hydrochloric acid, sulphuric acid, soda ash , sulphur and activated carbon and all these are manufactured in the country

### **1.4.7 Tamarind Seed**

Tamarind trees (*Tamarindus indica* ) are found naturalized almost throughout the plains and sub- Himalayan tracts of India. The pulp of tamarind fruits, known as imli, is used as an acid flavoring agent. The seeds constitute 34 percent starch of the fruits and contain on an average 60 percent starch, Statistical information on the annual production of fruit pulp and seeds is not available.



## **MARKET SURVEY**

### Growth in processed food industry vis-a-vis starch industry

The processed food industry is mainly unorganized with 75% of the processing units belonging to the unorganized category, the organized category though small, is growing fast. The food production is expected to double in the next 10 years and the consumption of value-added food products is expected to grow at a much faster pace. The share and growth of value-added products is likely to be higher going forward as companies in the processing sector opt for higher margin products on ample supply of raw materials used for starch for food additives.

The Indian organized starch industry has an estimated size of around Rs 3,500 crore. The Indian starch Industry is predominantly based on corn, with negligible usage of wheat. Out of more than 1,000 downstream applications of starch, 40 have been commercialized in India. With companies globally focusing on innovations in their product portfolio through R&D, the demand for starch sweeteners and other derivatives has picked up in a number of industries in India as well as in the international markets. During the period 2011-12, the Indian starch industry grew at a CAGR of 21.8%; while starch demand grows at around 5% per annum.

Gujarat with a strong agricultural base, 3.6 million hectares of irrigated land and well developed agro research capabilities is well positioned to drive the growth of food processing industry. Gujarat offers a large number of incentives to set up food processing units. Hassle-free policies such as single window clearance, a strong agricultural marketing network with over 200 Agriculture Produce Marketing Committees (APMCs) and over 110 cold storages are some of the enablers that have facilitated the rapid growth of this industry. The state also provides financial incentives by offering interest subsidies to agro-industrial units and air & sea freight subsidies for agro exports.

Starches, modified starches and their application find great relevance in the rapidly developing and growing Indian food processing industry. The demand is likely to grow in coming years with already established mega food parks and upcoming projects in India. To tap opportunities in this industry, Anil Ltd has formed SPV for setting up Gujarat's first mega food park. In the first quarter of 2011-12, Ministry of Food Processing Industries (MoFPI), Government of India, allotted the project of establishing mega food park at Savli near Vadodara to this SPV.

Starch and Glucose are reserved carbohydrates of plants and are therefore widely distributed in their crude form. They can be found in almost all fruits, vegetables and cereals. There is no definite information as to how they were initially obtained. But different countries are known to be using different agricultural sources for production of starch. While Japan and the European countries produce starch from potatoes, America from corn, countries like Thailand, and Brazil are understood to be producing starch mainly from tapioca. In the case of India, starch is being produced from Maize as well as tapioca. While the units producing starch from maize are concentrated in the large sector, the units producing starch from tapioca are by and large concentrated in the small scale sector.

Commercially glucose is produced from starch only and these two products are generally made in the same unit side by side.

The objective of this article is to discuss the present status, imports, exports and also the future prospects for both starch as well as liquid glucose.

<b>All-India Area, Production and Yield of Maize alongwith coverage under Irrigation</b>				
			Area - Million Hectares	
			Production Million Tonnes	
			Yield - Kg /Hectare	
Year	Area	Production	Yield	Area Under Irrigation(%)
1	2	3	4	5
2002-03	6.64	11.15	1661	19.5
2003-04	7.34	14.98	2041	19.1
2004-05	7.43	14.17	1907	20.5
2005-06	7.59	14.71	1938	21.1
2006-07	7.89	15.10	1912	21.5
2007-08	8.12	18.96	2335	23.5
2008-09	8.17	19.73	2414	25.2
2009-10	8.26	16.72	2024	NA
2010-11*	8.49	21.28	2507	NA
2011-12**	7.27	15.86	2181	NA

\* Fourth Advance Estimates as released on 19.07.2011.  
 \*\*First Advance Estimates released on 14.09.2011.  
 Note : The yield rates given above have been worked out on the basis of production & area figures taken in '000 units.  
 Source: Directorate of Economics and Statistics, Department of Agriculture

**Area, Production and Yield of Maize during 2009-10 and 2010-11 in major Producing States  
alongwith coverage under irrigation**

State	2010-11		2009-10		Area - Million Hectares		Production - Million Tonnes		Yield - Kg./Hectare		Area Under Irrigation (%) 2010-11*
	Area	% to All-India	Production	% to All-India	Area	% to All-India	Production	% to All-India	Yield		
	1	2	3	4	5	6	7	8	9	10	
Karnataka	1.24	15.01	3.01	18.02	2430	1.07	13.08	3.03	16.35	2835	41.3
Andhra Pradesh	0.78	9.48	2.76	16.62	3527	0.85	10.42	4.15	21.31	4873	49.4
Maharashtra	0.79	9.61	1.03	10.93	2302	0.66	8.01	1.56	7.91	2382	14.7
Bihar	0.63	7.55	1.48	8.84	2341	0.64	7.84	1.71	8.69	2676	60.6
Rajasthan	1.10	13.28	1.15	6.75	1044	1.05	12.88	1.83	9.27	1736	1.3
Tamil Nadu	0.24	2.96	1.74	6.84	4638	0.29	3.51	1.25	6.37	4389	47.9
Madhya Pradesh	0.83	10.07	1.08	6.25	1255	0.81	10.29	1.14	5.80	1381	1.8
Uttar Pradesh	0.71	8.58	1.04	6.21	1460	0.80	9.76	1.20	6.07	1495	34.5
Himachal Pradesh	0.30	3.58	0.54	3.25	1839	0.30	3.64	0.68	3.43	2273	8.8
Gujarat	0.60	6.02	0.63	3.19	1072	0.50	6.10	0.74	3.76	1481	9.6
Jammu & Kashmir	0.31	3.76	0.49	2.91	1556	0.32	3.66	0.63	3.21	2006	7.3
Punjab	0.14	1.58	0.40	2.31	3117	0.15	1.88	0.51	2.60	3104	61.6
West Bengal	0.10	1.18	0.39	2.30	3543	0.09	1.11	0.34	1.74	3762	17.4
Jharkhand	0.16	1.98	0.19	1.14	1155	0.22	2.64	0.30	1.54	1407	2.4
Others	0.43	5.17	0.65	3.88	@	0.41	4.98	0.64	3.23	@	
All India	8.26	100.00	16.72	100.00	2024	8.17	100.00	19.73	100.00	2414	25.2

@ - Since area's production is low in individual states, yield rate is not worked out.

Note: States have been arranged in descending order of percentage share of production during 2009-10.

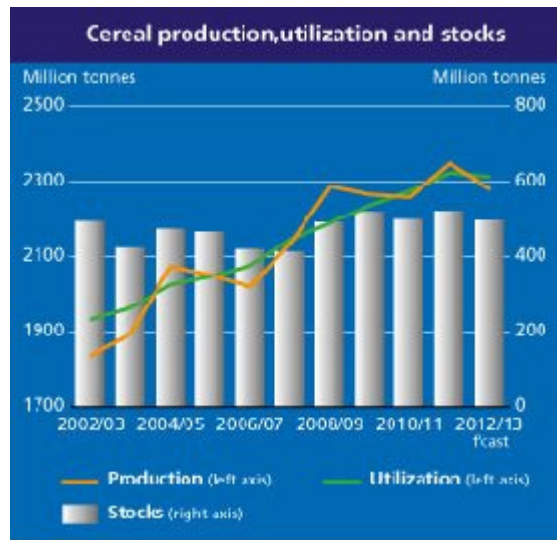
\* Provisional

Source: Directorate of Economics and Statistics, Department of Agriculture and Cooperation.

**UPPLY & DEMAND: MAIZE\***  
Million tons

	Opening stocks	Production	Imports	Total supply	Food	Industrial	Use Feed	Total a)	Exports	Closing stocks
<b>TOTAL COARSE GRAINS</b>										
2010/11	201.9	1,097.9	116.9	<b>1,299.8</b>	164.8	278.3	630.7	<b>1,127.2</b>	116.9	172.6
2011/12 <i>est.</i>	172.6	1,155.1	124.8	<b>1,327.8</b>	167.4	286.4	644.1	<b>1,156.9</b>	124.8	170.9
2012/13 <i>fcast</i>	170.9 (172.4)	1,120.7 (1107.8)	118.8	<b>1,291.6</b> (1280.1)	167.8	280.2 (277.6)	640.9 (627.6)	<b>1,143.5</b> (1128.8)	118.8	148.0 (151.4)
<b>MAIZE</b>										
<b>Argentina (Mar/Feb)</b>										
2010/11	1.7	22.7	0.0	<b>24.4</b>	0.3	1.4	4.5	<b>6.5</b>	16.0	1.9
2011/12 <i>est.</i>	1.9	23.8	0.0	<b>25.7</b>	0.3	1.4	4.7	<b>6.7</b>	15.7	3.3
2012/13 <i>fcast</i>	3.3	21.0	0.0	<b>24.3</b>	0.3	1.5	5.0	<b>7.1</b>	16.5	0.8
2013/14 <i>fcast</i>	0.8	27.5 (26.0)	0.0	<b>28.3</b> (26.8)	0.3	1.8	5.5	<b>7.9</b>	19.5 (18.0)	0.9
<b>Brazil (Mar/Feb)</b>										
2010/11	7.7	56.0	0.4	<b>64.1</b>	3.8	0.6	40.1	<b>46.9</b>	11.5	5.6
2011/12 <i>est.</i>	5.6	57.4	0.8	<b>63.8</b>	3.8	0.8	42.0	<b>48.9</b>	8.4	6.6
2012/13 <i>fcast</i>	6.6	73.0	0.5	<b>80.1</b>	3.9	1.3	43.2	<b>51.1</b>	21.0	8.0
2013/14 <i>fcast</i>	8.0 (10.0)	71.0	0.4 (0.3)	<b>79.4</b> (81.3)	4.0	1.7	45.0	<b>53.7</b>	18.0	7.7 (9.6)
<b>EU-27 (Oct/Sep)</b>										
2010/11	7.8	55.8	7.5	<b>71.0</b>	4.2	11.0	46.7	<b>64.1</b>	1.0	6.0
2011/12 <i>est.</i>	6.0	66.0	6.3	<b>78.3</b>	4.2	12.0	50.0	<b>68.6</b>	3.0	6.7
2012/13 <i>fcast</i>	6.7	54.2 (53.6)	10.5 (10.0)	<b>71.4</b> (70.3)	4.2	13.5 (13.3)	46.7 (45.8)	<b>66.5</b> (65.5)	0.8	4.1
<b>South Africa (May/Apr)</b>										
2010/11	3.7	13.4	0.0	<b>17.1</b>	4.3	0.1	5.1	<b>10.2</b>	2.1	4.8
2011/12 <i>est.</i>	4.8	10.9	0.3	<b>16.0</b>	4.3	0.1	5.4	<b>10.4</b>	2.4	3.2
2012/13 <i>fcast</i>	3.2	12.0	0.0	<b>15.2</b>	4.3	0.1	5.4	<b>10.4</b>	1.8	3.0
2013/14 <i>fcast</i>	3.0 (2.7)	13.0	0.0	<b>16.0</b> (15.7)	4.3	0.1	5.5	<b>10.5</b>	2.5	3.0 (2.7)
<b>Ukraine (Oct/Sep)</b>										
2010/11	0.7	11.9	0.0	<b>12.6</b>	0.4	0.3	5.2	<b>6.5</b>	5.0	1.1
2011/12 <i>est.</i>	1.1	22.8	0.0	<b>23.9</b>	0.4	0.3	6.0	<b>7.7</b>	15.1	1.1
2012/13 <i>fcast</i>	1.1	20.9 (20.0)	0.0	<b>22.0</b> (21.1)	0.5	0.3	6.2 (6.3)	<b>7.8</b> (7.9)	13.2 (12.0)	1.0 (1.2)
<b>USA (Sep/Aug)</b>										
2010/11	43.4	316.2	0.7	<b>360.3</b>	5.0	157.8	121.7	<b>285.0</b>	46.6	28.6
2011/12 <i>est.</i>	28.6	313.9	0.7	<b>343.3</b>	5.2	157.7	115.5	<b>279.0</b>	39.2	25.1
2012/13 <i>fcast</i>	25.1	273.8 (272.4)	2.5	<b>301.4</b> (300.0)	5.1	143.3	113.0 (105.0)	<b>262.1</b> (254.0)	24.1 (29.5)	15.3 (16.5)
<b>China (Oct/Sep)</b>										
2010/11	50.3	177.2	1.0	<b>228.6</b>	6.8	45.0	115.0	<b>174.7</b>	0.1	53.8
2011/12 <i>est.</i>	53.8	192.8	5.3	<b>251.9</b>	7.0	50.0	126.4	<b>192.9</b>	0.2	58.8
2012/13 <i>fcast</i>	58.8	208.0 (198.0)	2.0	<b>268.8</b> (258.8)	7.2	56.0 (53.0)	136.5 (131.0)	<b>209.6</b> (200.2)	0.2	59.0 (58.4)
<b>Japan (Oct/Sep)</b>										
2010/11	0.8	0.0	15.7	<b>16.4</b>	1.1	3.3	11.0	<b>15.7</b>	0.0	0.7
2011/12 <i>est.</i>	0.7	0.0	14.8	<b>15.5</b>	1.1	3.4	10.2	<b>14.9</b>	0.0	0.6
2012/13 <i>fcast</i>	0.6	0.0	14.9	<b>15.5</b>	1.1	3.4	10.1	<b>14.9</b>	0.0	0.6
<b>WORLD TOTAL</b>										
2010/11	145.4	829.6	93.3	<b>975.0</b>	95.7	242.0	474.9	<b>843.9</b>	93.3	131.1
2011/12 <i>est.</i>	131.1	876.9	96.8	<b>1008.0</b>	99.0	249.7	490.7	<b>875.4</b>	96.8	132.7
2012/13 <i>fcast</i>	132.7 (134.4)	844.7 (830.1)	93.4 (93.8)	<b>977.3</b> (964.5)	99.5	243.4 (240.4)	487.4 (475.6)	<b>864.6</b> (849.0)	93.4 (93.8)	112.7 (115.5)

## Lower cereal production and stocks from last month while trade forecast raised



### World cereal production in 2012 falls

FAO's latest forecast for world cereal production in 2012 has been revised downward marginally (2 million tonnes) since the November figure to 2 282 million tonnes (including rice in milled terms), 2.8 percent down from the previous year's record. This month's revision mostly reflects adjustments to maize output estimates in the Russian Federation and Ukraine, where figures became firmer towards the completion of the harvests, as well as reduced wheat production prospects in Australia and Brazil where the 2012 harvests are underway. Prospects for rice production in 2012 remained virtually unchanged. Based on latest figures, the overall decrease in world cereal output this year comprises a 5.7 percent reduction in wheat production and a 2.6 percent decline for coarse grains, which largely outweighed the marginal 0.9 percent growth expected in the global rice crop. Early indications for the winter wheat crops already planted in the northern hemisphere, to be harvested in 2013, are mixed, and somewhat less promising than one month ago. Although firm estimates are not yet available, latest information suggests that farmers generally responded to the incentive of high prices by increasing their winter wheat plantings. However, conditions remain adversely dry for emergence and crop establishment before dormancy in important producing regions of the United States and the Russian Federation, while in major producing parts of the EU, wet conditions have hampered fieldwork.

### **Total cereal utilization in 2012/13 down slightly from 2011/12**

» World cereal utilization in 2012/13 marketing season is forecast at 2 314 million tonnes, nearly unchanged from the previous month and down slightly (0.4 percent) from the previous season. The anticipated reduction from 2011/12 would be on account of reduced feed use of wheat and industrial usage of maize. Total use of cereals for food consumption is forecast to rise by 1.3 percent in 2012/13, keeping pace with world population growth and therefore resulting in a stable per capita consumption of 152.6kg for the world as a whole. A slight increase foreseen in rice consumption (on per caput level) is expected to offset a small decline in wheat. As for the global utilization, in the case of wheat it is forecast to contract by 1.2 percent in 2012/13 to 686 million tonnes, reflecting a 5.8 percent cut in the use for wheat for animal feed from the previous season's all-time high to 138 million tonnes. Lower feed use of wheat in China (from a record in 2011/12) and the EU is expected to more than compensate for the significant (almost 4 million tonnes) increase in feed use of wheat in the United States, which could hit a new record because of elevated maize prices. Total utilization of coarse grains is also forecast down, by 0.8 percent, from the previous season, to 1 152.2 million tonnes. While feed use of coarse grains is likely to increase slightly (0.5 percent) to 638 million tonnes, its industrial application is seen to contract sharply, mainly reflecting a significant (10 percent) reduction in demand from the ethanol industry in the United States, the world's largest maize-based ethanol producer.

### **Falling wheat and coarse grain inventories against rising rice stocks**

The latest forecast for world cereal stocks at the close of crop seasons ending in 2013 stands at around 495 million tonnes, down 5 percent (25 million tonnes) from their opening level. This forecast is slightly (0.6 percent) below the November figure, mainly because of revisions to wheat stock levels. At the current forecast level, the world cereal stock-to-use ratio is projected at 20.5 percent, down 2 percentage points from 2011/12 and only 1.7 percentage points above the 2007/08 low of 18.8 percent. World wheat inventories are expected to fall to 163 million, down 11 percent from their opening level and 2 percent (3 million tonnes) less than was reported in November. The revision since the previous month largely reflects lower anticipated inventories in China and India, more than offsetting a small increase in the United States. The sharp reduction from the previous season is mostly on account of reduced stocks in the CIS countries (because of disappointing harvests), China (driven by strong domestic use), the EU (following a decline in production) and the United States (reflecting a surge in domestic feed use). World inventories of coarse grains are forecast to exceed 161 million tonnes, 8 percent (15 million tonnes) less than their opening level and nearly unchanged from November. Most of the decline from the previous season reflects shrinking inventories in the United States, where total coarse grain inventories are projected down nearly 8.3 million tonnes while significantly lower (by 4.6 million tonnes) stocks are also forecast for the EU. By contrast, global rice inventories are expected to increase by 6.6 percent (10.5 million tonnes) to a record of nearly 170 million tonnes, unchanged from the previous month. This expansion reflects three consecutive years of record world production.

## **NAME AND ADDRESS OF MANUFACTURERS OF LIQUID GLUCOSE**

### **STARCH**

Mg. Director  
AMAR CHEMICALS  
P.O. Box 55,  
Amar Talkies Bldg.  
Dhamtari-493773,  
Madhya Pradesh  
Phone: 07722-237277  
Email: amarchem@vsnl.com

Mr. C. D. Patel  
ANIL PRODUCTS  
302, Prabhat Kiran,  
Rajendra Place  
New Delhi-110008  
Phone: 011-25863811/12

Mr. Ashish Shah  
ANIL PRODUCTS LTD  
Contractor Bldg., 1st Floor,  
Ramjibhai Kamani Marg  
Mumbai-400038, Maharashtra  
Phone: 022-22614075/6  
Email: anil\_rob@yahoo.com

Shripal C. Sheth, Director  
ANIL STARCH MARKETING LTD  
Anil Road, Ahmedabad-380025,  
Gujarat  
Phone: +91 79 212 3222



## **LIQUID GLUCOSE**

MR. K. GOPALKRISHNAN  
D S Q BIOTECH LTD  
40, BAZULLAH ROAD  
1ST FLOOR, T. NAGAR  
CHENNAI-600017, TAMIL NADU  
Phone: 044-28228155/8204/28206420-22

V. RAJKUMAR, JT. M.D.  
KAMALA SUGAR LTD  
GOWTHAM CENTRE ANNEXE,  
1054/14 & 15, 1ST FLOOR, AVAN  
COIMBATORE-641018, TAMIL NADU  
Phone:+91 422 572 132

MR. NARENDRA D  
L N EXIM PVT LTD  
108, TWIN ARCADE,  
'C' ING, MILITARY ROAD,  
MAROL, ANDHERI (E),  
MUMBAI-400059, MAHARASHTRA  
Phone: 912256924113/14/28503533/56205802/65205802  
Email: lnexim@vsnl.net

MR RAJEEV NANDA  
MAHALAXMI MAIZE PRODUCTS  
C/69, 2ND FLOOR,  
B G TOWER, SHAHIBAUG ROAD,  
AHMEDABAD-380004, GUJARAT  
Phone: 917925622134/25633854  
Email: ravjeevnanda@hotmail.com

## **LIST OF MANUFACTURERS OF RAW MATERIAL-DEXTROSE**

JAGDISH MACHINERIES PVT LTD  
3, Sharada Industrial Estate,  
Near Picker'S Factory,  
Anil Starch Road ,Saraspur  
Ahmedabad-380018, Gujarat  
Phone: 079-2201455

S. V. Shanmuga Vadivelu, Director  
RIDDHI-SIDDHI GLUCO-BIOLS LTD  
701, Sakar - I, Off. Ashram Road  
Ahmedabad-380006, Gujarat  
Phone: +91 79 658 1000  
Email: sdroy\_rsgbl@rediffmail.com

SUKHJIT STARCH & CHEMICALS LTD  
Sukhjit Road  
Phagwara-144401, Punjab  
Phone: +91 1824 261 516,  
+91 1824 262 144, +91  
Email: sukhjit@comeconnect.com  
sukhjit@vsnl.com

UNIVERSAL PROCESS ENGINEERS  
Plot A28/1/10, I.D.A, Nacharam  
Hyderabad-500076, Andhra Pradesh  
Phone: 040-7172573  
Email: upe040@yahoo.com

UNIVERSAL STARCH CHEM ALLIED LTD  
Mhatre Pen Bldg., `B Wing , 2nd Floor,  
Senapati Bapat, Marg Dadar (W)  
Mumbai-400028, Maharashtra  
Phone: 022-24300898  
Email: usaltd@bom3.vsnl.net.in

## **MANUFACTURES OF STARCH AND ALLIED PRODUCTS**

### **Maize Starch**

Starch from maize is obtained by the wet milling process. The process involves cleaning of grains, steeping, milling, separation of husk, germ and gluten, and drying the product. The grains received at the mills and magnetic separators to completely eliminate the extraneous matter present. The cleaned grain is stored in concrete silos.

The grain is transported to steeping vat by elevators and conveyors through a weighing machine. Warm water containing a small amount of sulphur dioxide is circulated through the vats to loosen the husk and soften the gluten. During the steeping, a part of the soluble salts and proteins of the grain get dissolved and when the solid matter content of the water reaches percent at 6-10 it is replaced by fresh steep water. Washed water is concentrated by evaporation and is used as cattle feed.

After steeping the softened grains are passed over vibrating screens to remove any adhering foreign matter and then ground in attrition mills consisting of two plates with producing teeth. The ground mass is passed in to wooden, V shaped, germs from the rest of the mass. The floating terms are skimmed over by sweep paddles, washed on screens dried and sent to the oil extraction plant. The mixture of starch gluten, husks and fibre recovered at the bottom and sent to vibrating screens to eliminate excess water and soluble substances. It is then thoroughly milled in fine grinders to fine slurry known as starch milk. The grinders may be either Buhrer stone mills or preferably vertical mill made of stainless steel. The starch milk is processed in centrifuges to remove husk and fibre which are washed free of adhering starch in the counter current system and washing fed back to the main starch stream.

The resulting slurry is passed through high speed continuous centrifuges where the lighter gluten is separated from the heavier starch. In the first stage, the heavy starch layer is tapped in such a way that least possible amount of starch goes in which the overflow of gluten, thus maintaining gluten purity. In the latter stages the process is reversed to ensure the purity of the starch. The gluten from the first stage is concentrated and pressed into cake. The glutenous starch from the latter stages is fed back to the main stream at the husk separation stage. The deglutenized starch milk is dewatered in a perforated bucket centrifugal machine to a moisture content of about 30-36 percent. It is flash-dried and packed or passed on to other division for the manufacture of starch derivatives (Information from the Anil Starch products at Ahmedabad).

## **TAPIOCA STARCH**

In raw tapioca tuber amount 20-30 percent of the weight account for starch while the remainder is made up of fibre, water, other carbohydrates and proteins. The method of extracting tapioca starch is essentially similar to the maize starch. It is however comparatively simpler owing to relatively small amount of secondary substances in tapioca. To obtain a good product, processing of tapioca tuber after digging should be accomplished within the shortest possible period to avoid the enzymic activity.

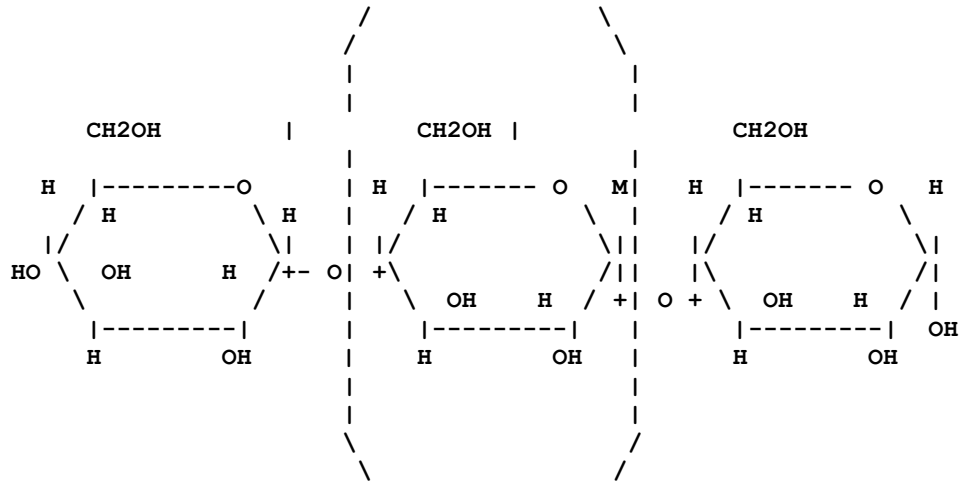
The method involves peeling, rasping, straining, recovery of starch granules and drying. In small units, the tubers are peeled by hand and then washed in water. In large units whole roots are processed in compartment washer consisting of perforated tank equipped with water jets and horizontal shaft with paddles to agitate the tubers.

Here the roots are thoroughly agitated and washed with water so that all the dirt and a good portion of the peel are removed. In small scale units rasping is done by pressing the tubers against the sharp projection of a wheel grater operated by hand, treadle or machine. Large units use a John Resper, a machine consisting of a rotor fitted with several saw blades; the shape and number of teeth on each blade determines the efficiency of separation of starch granules. The percentage of starch set free by rasping determines to a large extent the commercial success in the manufacturing of starch.

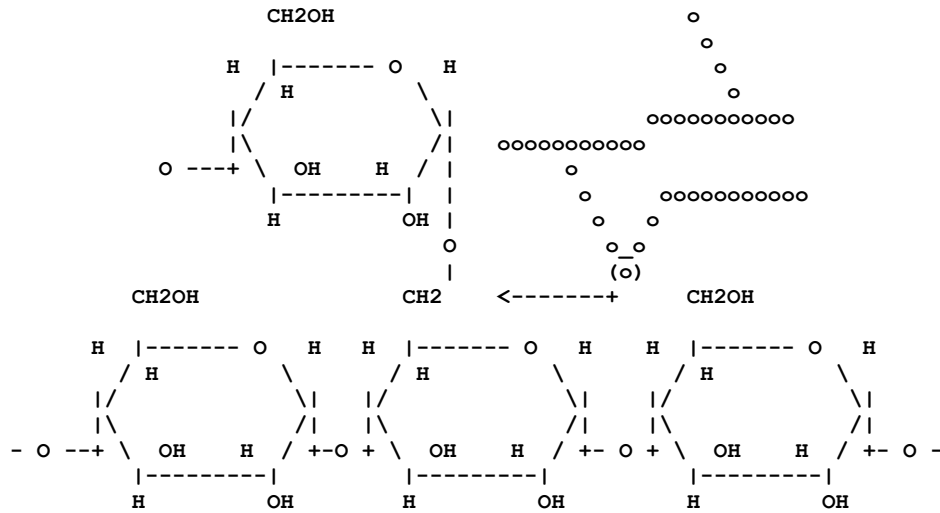
The rasped material is strained with water to liberate the starch granules from the fibrous residues. In the small units this is done by squeezing in coarse bages or frames fitted with violuor mill (Cotton fabric). In large units the diluted pulp is passed through a battery of rotating and shaking screens of increasing fineness (80-200). The residue on the first screen is returned for a second rasping.

The starch milk obtained by straining is treated for the recovery of starch granules in various ways. Pot settling is in vogue in cottage industries while settling on table is common in small scale units. In large units, this operation is carried out rapidly by means of centrifugal separators and purifiers. The starch slurry obtained by settling is then partly dewatered on centrifuges and vacuum filters. Final drying of starch is done in chamber kiln or flash driers working on steam or hot air. In small units it is sun-dried working on steam or hot air. In the small units it is sun-dried. If in lump form the dried starch is pulverized and bolted (dry screening) before packing (Information from the Laxmi Starch Factory Ltd, Kundara).

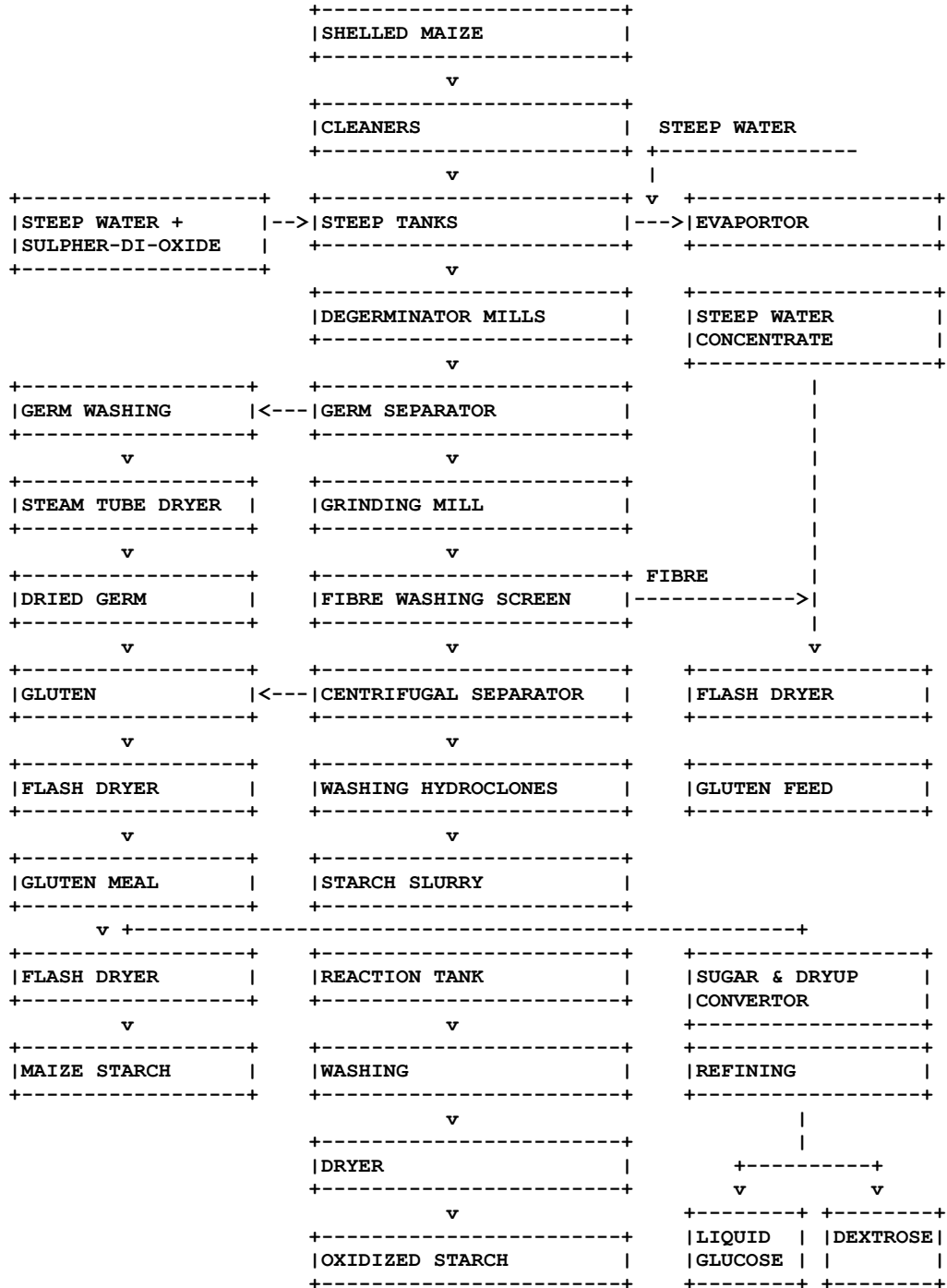
**AMYLOSE MOLECULE OF STARCH**  
**TABLE NO.2.1**



**AMYLOPECTIN MOLECULE**



## PROCESS FLOW DIAGRAM FOR THE MFG. OF STARCH



## **MANUFACTURING PROCESS FOR LIQUID GLUCOSE-G**

The raw materials required for the manufacture of glucose are starch and mineral acid; Amylolytic enzymes may also be use for starch hydrolysis. The conversion of starch to glucose takes place through a series of steps in which carbohydrates of progressively decreasing complexity-soluble starch, dextrim like amylo dextrin, erythro dextrin and achro-dextrin, maltose and dextrose- are formed. The composition of the hydrolysate is determined largely by the concentration and temperature of the acid used for catalysing the hydrolysis. For the manufacture of glucose a starch suspensions in water containing 35-40% starch is mixed with sufficient hydrochloric acid to give a concentration of 0.012 to 0.02N acid in the final mixture and heated in an autoclave to a temperature of 140-160. The product is held at this temperature for 15-20 minutes. The reaction mixture is tested with iodine and if not starch is present, as indicated by the colour test the pressure is released and the liquit transferred to a neutralizing tank. The acid is neutralized with soda ash. Proteins fats, fatty acids, and colloidal material are coagulated by adjusting the PH to 4-3. The mixture is passed through a filter press, the filtrate is decolourised by activated carbon and the clear filtrate clear filtrate concentrated in a triple offect evaporator. Treatment with activated carbon is repeated and the liquid further concentrated in a vacuum pan. The concentrated syrup (40-45~ Be) is quickly cooled and tranferred to drums. The product obtained contains 43% dextrosion dry basis. Glucose is prepared also by enzymic conversion of starch or by a combination of acid conversion, neutralisation and enzymic conversions (U.S. Patent 2,201,609 of 1940)

### **RAW MATERIALS**

The principal raw materials required for the manufacture of glucose is starch. Excepting glucose and foods Ltd. who purchase their requirement of maize starch, other factories utilize upto 20% of their any productions of maize starch. Maize was being imported from U.S.A. for making starch but the price of maize was reported to be somewhat higher than that of imported starch. Efforts have been made to use indigenous tapioca starch as the raw material. In fact Kamla Sugar Mills Ltd. have attempted to utilize only tapioca starch for the manufacture of dextrose.



The manufacturing process employed in India is the same as that in use in other countries. Maize starch is suspended in water and cooked after adding hydrochloric acid, in a converter under a pressure of 30 lbs/inch. For 15 minutes the hydrolysis is interrupted when a test sample of the hydrolysate fails to give a blue coloration with iodine. The pressure is released and the charge run into a wooden vat, where it is neutralised with a solution of soda ash and the reaction adjusted to the Iso electric point to coagulate colloidal impurities. The liquor is filtered decolorized with activated carbon and filtered again. The filtrate (20~ Be) is concentrated to 30-32 Be under vacuum, when all inorganic salts other than sodium chloride precipitate out. The syrup is treated with activated carbon, filtered, and concentrated to 45 Bc. It is then cooled packed in steel drums or in galvanised tin containers of 56 lb capacity. Both ordinary and B.P. liquid glucose are manufactured in India. The former contains 43-44% reducing sugars (estimated as dextrose) the B.P. product contains 43-47% reducing sugars. The quality of indigenous liquid glucose is reported to be satisfactory though there appears to be scope for improvement.

#### **CONFECTIONERY GLUCOSE-D:**

Confectionery glucose, otherwise known as syrup (when derived from maize) crystal syrup, commercial glucose is a highly viscous, slightly sweet and colourless substance. It is produced in a wide range of beam densities, 26~ - 45~ approximately, and an equally comprehensive range of dextrose equivalent, or D.E. of glucose syrup is a factor, calculated on a dry basis which provides a guide as to the amount of fermentable sugars present liquid glucose is chiefly derived from maize, and, to a lesser degree potato starches.

The process of manufacture is based on hydrolysis of refined starches under several atmospheres of pressure in the presence of a minute quantity of chemically pure hydrochloric acid. The hydrolysed syrup is neutralised and purified with the aid of animal or activated carbon. This carbon treatment is analogous to the methods used in the refining of cane or beet sugar.

The degree of hydrolysis of liquid glucose is closely controlled, and modified to produce a final syrup possessing the required dextrose equivalent the beam density is of course dependent on the degree of evaporation in vacuo.

Normal liquid glucose contains simply expressed dextro maltose dextrin and water and has the following approximate analytical characteristics, at 43~Be density.

1. Water	17.7
2. Dextro and maltose expressed as dextrose d.b.	35.0
3. Ash	0.40
4. Polysaccharides	46.85
5. Sulphur Dioxide	0.03

Under the food and Drugs. Regulations, liquid glucose is permitted to contain a maximum of 450 parts per million sulphur dioxide as a preservative, actually in practice it contains approximately 350-400 p.p.m.

Liquid glucose may be classified into four main groups based on the degree of conversion, and sub-divided by the method of conversion into a further two groups, i.e. single conversion and dual conversion. The difference between the two methods is that an additional converting agent, an appropriate enzyme, is employed after the single acid conversion process has taken place, hence the term "dual".

#### **LOW CONVERSION:**

Syrups of a D.E. of less than 40 are considered low conversion types.

#### **REGULAR CONVERSION**

The next D.E. range, from 40-49, includes liquid glucose of the type normally used. The syrups in this range contain 62-63% total sugars on a dry solids basis, and are usually offered at D.E. 42.

## **INTERMEDIATE CONVERSION**

These syrups are in the 50-57 D.E. range and are produced by single and dual conversion. The total sugar solids are of the order of 70.3 - 78.3%

## **HIGH CONVERSION**

These glucose syrups fall in the D.E. 58.64 and over range the total sugar solids are 84 - 87.8%. They contain the smallest proportion of polysaccharides, and have the highest fluidity, hence their humectant characteristics. The manufacture of liquid glucose, a highly complex substance, is subject to the most exacting production and analytical control so that it will perform its proper function of granulation inhibition prolongation of shelf life, and several other essential effects in the sugar confectionary field.

**TURNKEY CONSULTANT FOR SETTINGUP MAIZE PROCESSING UNIT**

K. SIVA REDDY,  
Chief Consultant,  
S.S.STARCH CONSULTANCY.  
FLAT # 406 S, BANKER CHAMBER,  
A.S.RAJUNAGAR, KUKATPALLY,  
HYDERABAD-500072, INDIA.  
Mobile # +919440076510 or 9866581999.  
Email : ssstarchconsul@yahoo.com  
ssstarchprocessors@yahoo.com  
ssstarchconsul@gmail.com  
ssstarchprocessors@gmail.com  
Website : www.ssstarchconsultancy.in or www.ssstarchconsultancy.com

Favorich,  
#45/3, JD Royallite,  
Tumkur Road, Yeshwanthpur,  
Bangalore-560022.  
Tel:+91-80-23577111  
FAX:+91-80-23577555  
Email:fapl@favorichindia.com

PRAJ INDUSTRIES LTD.  
Head Office  
Address :Praj House, Bavdhan,  
Pune 411 021. INDIA  
Tel :+91-20-22951511 / 22952214  
+91-20-39806666 / 22905000  
Fax :+91-20-22951718 / 22951515  
e-mail :info@praj.net

STARCH CHEM Consultant & Engineers Pvt. Ltd.  
15, Nichaldas Market,  
Sindhi Society, Chembur,  
Mumbai - 400 071 (India)  
Tel: 65751611,25220478  
Tele/ Fax: 91 22 25277428  
mail to : starchchem@vsnl.net

### **List of some starch processing industries**

- Sukhjit Starch & Chemicals Ltd., India.
- Bharat Starch & Chemicals Ltd., India- Thaper Group.
- Rajaram Brothers, India.
- K.G.Gluco Biols Ltd., India-Joint Venture Glaxo (India) & Karnataka State Industrial Development Corporation.
- Kashyap Sweetners Ltd., India.
- Anil Starch Products Ltd., India.
- Laxmi Starch Ltd., India.
- Sahyadri Starch & Auxichem Pvt.Ltd., India.
- Shri Devji Agro Industries Pvt.Ltd., India.
- Gayatri Starchem Industries Ltd., India.
- Wave Industries., India.
- Shri Sangam Glucose Ltd., Pune, India

**COMPLETE PLANT AND MACHINERY SUPPLIERS FOR STARCH (MAIZE)**

Sifter International  
Corporate Office :  
Plot No. 227, Sector - 24,  
Faridabad- 121005, Haryana (INDIA)  
Phone :+91-129-4060039 / 2234540  
Telefax : +91-129-2230039  
E-mail : sifter@ndb.vsnl.net.in

UNIVERSAL PROCESS ENGINEERS PVT. LTD.  
Address PLOT NO. A28/1/10, I.D.A, NACHARAM,  
Hyderabad - 500076, Andhra Pradesh, India  
Phone No 91-40-27172573  
Fax 91-40-27179701  
Contact Person Mr. SYED ISMAIL (Managing Director)  
Mobile +919849052100

## **SUPPLIERS OF RAW MATERIALS**

### **HYDROCHLORIC ACID**

Hind Enterprises

10/ 12, Narayan Niwas, Office No. 10,  
3rd Floor, Opposite Edward Cinema,  
Jamboolwadi, Kalbadevi Road,  
Mumbai - 400002, Maharashtra, India  
Phone: +(91)-(22)-22058743  
Website: <http://www.hindenterprises.net/>

Lords Chloro Alkali Limited

A-263, IInd Floor, Defence Colony,,  
New Delhi - 110 024, Delhi, India  
Phone: +(91)-(11)-46865999  
Website: <http://www.lordschloro.com/>

Water Care Technology

L-121/122, Ground Floor,  
Phase 2,, New Delhi - 110001  
Phone: +(91)-(11)-27512220  
Preferred Number: 08373902939  
Website: <http://www.swimmingpoolexpertindia.com/>

## **SULPHURIC ACID**

Triveni Chemicals

No. 135, Pancharatna Char Rasta,  
G. I. D. C., Vapi, Gujarat - 396 195, India

Phone: +(91)-(260)-6618618

Fax: +(91)-(260)-6618624

Mobile / Cell Phone: +(91)-9227788155

Website: <http://www.trivenichemical.com/chemicals-by-alphabet-s.html>

Surya Fine Chem

C/102 Sai Grece, Near Eagle Hotel  
PCMC Link Road, Near Petrol Pump, Pune,

Maharashtra - 411 033, India

Phone: +(91)-(20)-65103846

Mobile / Cell Phone: +(91)-9890443743

Website: <http://www.suryafinechem.com/laboratory-chemicals.html>

## **SODA ASH**

Triveni Chemicals

No. 135, Pancharatna Char Rasta,  
G. I. D. C., Vapi, Gujarat - 396 195, India

Phone: +(91)-(260)-6618618

Fax: +(91)-(260)-6618624

Mobile / Cell Phone: +(91)-9227788155

Website: <http://www.trivenichemical.com/chemicals-by-alphabet-s.html>

B. K. Chemicals

B - 2, Shrushti Apartment, 1st Floor, Near Century Enka,  
Colony No. 2, Pune - Nasik Highway, Bhosari,

Pune, Maharashtra - 411 039, India

Fax: +(91)-(20)-27111941

Mobile +(91)-9371020040 / 9881418345

Website: <http://www.bkchemicals.in/industrial-chemicals-powder.html>



Yash Chemicals

Shop No D -31, Gagan Avenue, Near Sai Service,  
Kondhwa - BK, Pune, Maharashtra - 411 048, India

Phone: +(91)-(20)-26930858

Fax: +(91)-(20)-26930858

Mobile / Cell Phone: +(91)-9372286769 / 9822286769

Website: <http://www.yashchemicals.net/>

### **CAUSTIC SODA**

B. K. Chemicals

B - 2, Shrushti Apartment, 1st Floor,  
Near Century Enka, Colony No. 2,  
Pune - Nasik Highway, Bhosari, Pune,  
Maharashtra - 411 039, India

Fax: +(91)-(20)-27111941

Mobile / Cell Phone: +(91)-9371020040 / 9881418345

Website: <http://www.bkchemicals.in/industrial-chemicals-powder.html>

Triveni Chemicals

No. 135, Pancharatna Char Rasta,  
G. I. D. C., Vapi, Gujarat - 396 195, India

Phone: +(91)-(260)-6618618

Fax: +(91)-(260)-6618624

Mobile / Cell Phone: +(91)-9227788155

Website: <http://www.trivenichemical.com/chemicals-by-alphabet-c.html>

## **ACTIVATED CARBON**

Air Care Equipments

Dreams Aakruti, C-102, Plot No-1, Sr. No.-52,  
Kalepadad, Near Dhere Concrete Company,  
Hadapsar, Pune, Maharashtra - 411 028, India

Phone: +(91)-(20)-24345758

Fax: +(91)-(20)-24345758

Mobile / Cell Phone: +(91)-9823050371 / 9420174854

Website: <http://www.aircarepune.com/>

Hindustan Produce Company

No. 7, Clyde Row, Hastings, Kolkata,  
West Bengal - 700 022, India

Phone: +(91)-(33)-22230828 / 22230110

Fax: +(91)-(33)-22230140

Mobile / Cell Phone: +(91)-9831484682

Website: <http://www.hindustanproduceco.com/petroleum-coke-graphite-powder-flakes-activated-carbon.html>

## PLANT & MACHINERY SECTION WISE

### A. List of machinery and equipment

#### 1. Maize Steeping

1.01	8	<u>Steeping tanks</u> For maize steeping.	Approx. 150 M3 each. RCC - Customer scope
1.02	1	<u>Tank</u> To provide suction head for the maize pump,	Approx. 0.5 M3 Stainless steel 316
1.03	8	<u>Centrifugal Pumps</u> To circulate steeping water	Approx. 40 M3 / each Approx 20 M Stainless steel 316
1.04	8	<u>Heat Exchangers</u> To heat the circulating steeping water	Approx. 2 M3 / each Stainless steel 316
1.05	1	<u>Centrifugal Pump</u> To pump and steeped maize and flushing water to the maize dewatering screen.	Approx. 70 M3 / hr Approx 20 M Stainless steel 316
1.06	<u>1</u>	<u>Arc Screen</u>	



## 2.Sulphurdioxide Plant

2.01	1	<u>Sulphur Burner with all Accessories</u> For Sulphur combustion. Capacity Material	Approx. 25 Kg/h, Carbon steel, cast iron.
2.02	1	<u>Compressor with Air Receiver</u> To provide combustion air to Sulphur burner. Capacity Material	Approx. 500 Nm <sup>3</sup> /h, CI
2.03	1	<u>Absorption tower</u> For absorption of sulphur gas.  Diameter Height Material Packing	Approx. 0.6 M Approx. 6 M Stainless steel 316 Structured packing
2.04	1	<u>Centrifugal Pump</u> For SO <sub>2</sub> - water  Capacity Delivery head Material	Approx. 12 M <sup>3</sup> /h Approx. 20 M Stainless steel 316
2.05	1	<u>Tank</u> For SO <sub>2</sub> - water  Volume Material	Approx. 60 M <sup>3</sup> FRP
2.06	1	<u>Centrifugal Pump</u> For SO <sub>2</sub> - water  Capacity Delivery head Material	Approx. 40 M <sup>3</sup> /h Approx. 30 M Stainless steel 316
2.07	1	<u>Plate Heat Exchanger.</u> for SO <sub>2</sub> water.  Material	SS 316

### 3. Degermination and Germ Washing

- 3.01 1 Tank  
For Dewatered steeped maize.  
Volume Approx. 7.5 M<sup>3</sup>  
Material Stainless Steel 316
- 3.02 1 Rotary Valve  
To meter steeped maize into the 1st grind mill..  
Capacity Approx. 12 T/h maize  
Material Stainless steel 316
- 3.03 1 1st Grind Mill  
steeped  
For coarse milling of maize.  
Capacity 500 MT/Day maize equivalent  
Material Stainless Steel 316
- 3.04 1 Tank  
For Coarse milled maize slurry  
Volume Approx. 7 M<sup>3</sup>  
Material FRP
- 3.05 1 Agitator  
To mix coarse milled maize slurry.  
Material Stainless Steel 316
- 3.06 1 Centrifugal Pump  
To pump coarse milled maize slurry to the first  
stage germ hydrocyclone unit.  
Capacity Approx. 65 M<sup>3</sup>/h  
Delivery head Approx. 70 M  
Material Stainless steel 316

3.07	1	<p><u>1st Stage germ hydrocyclone unit.</u> To separate maize germ by centrifugal flotation, 1st stage consists of 2 sets of hydrocyclones</p> <p>Capacity 500 MT/Day maize equivalent.</p> <p>Material Stainless steel 316</p>
3.08	1	<p><u>Arc Screen.</u> To dewater partially milled and degerminated maize slurry.</p> <p>Material Stainless steel 316</p>
3.09	1	<p><u>2nd Grind Mill</u> For milling of partly degerminated maize slurry.</p> <p>Capacity 500 maize MT/Day equivalent.</p> <p>Material Stainless steel 316</p>
3.10	1	<p><u>Tank</u> For fine milled maize slurry</p> <p>Volume Approx. 7 M<sup>3</sup></p> <p>Material FRP</p>
3.11	1	<p><u>Agitator</u></p> <p>Material Stainless Steel 316</p>
3.12	1	<p><u>Centrifugal Pump</u> To pump fine milled maize slurry to the 2nd stage germ hydrocyclone unit.</p> <p>Capacity Approx. 65 M<sup>3</sup>/h Approx. 70 M</p> <p>Material Stainless steel 316</p>
3.13	1	<p><u>2nd Stage germ hydrocyclone unit.</u> To separate maize germ by centrifugal flotation, 2nd stage consists of 2 sets of hydrocyclones.</p> <p>Capacity 500 MT/Day maize equivalent.</p> <p>Material Stainless steel 316</p>

3.14	3	<u>Germ washing arc screens</u> For counter current washing of maize germ, Material Stainless steel 316
3.15	1	<u>Agitator</u> To mix content of overflow pit. Material Stainless Steel 316
3.16	1	<u>Centrifugal Pump</u> To pump germ wash water from one screen to the next Capacity Approx. 20 M <sup>3</sup> /h each Delivery head Approx. 20 M Material Stainless steel 316
3.17	1	<u>Tank</u> As overflow pit to collect any overflows. Volume Approx. 15 M <sup>3</sup> Customer's scope Concrete with epoxy resin coated.
3.18	1	<u>Tank</u> For Germ Milk. Volume Approx. 4 M <sup>3</sup> Material FRP
3.19	1	<u>Centrifugal Pump</u> To pump contents of overflow pit to the 1st grind tank. Capacity Approx. 7 M <sup>3</sup> /h Delivery head Approx. 20 M Material Stainless steel 316



#### 4. Fibre Milling And Washing

4.01	1	<u>Tank</u>	
		For Degerminated maize slurry	
		Volume	Approx. 3 M <sup>3</sup>
		Material	FRP
4.02	1	<u>Agitator</u>	
		For maize slurry tank	
		Material	Stainless Steel 316
4.03	1	<u>Centrifugal Pump</u>	
		For maize slurry	
		Capacity	Approx. 30 M <sup>3</sup> /h
		Delivery head	Approx. 40 M
		Material	Stainless steel 316
4.04	1	<u>Pressure fed arc screen</u>	
		For fibre dewatering	
		Material	Stainless steel 316
4.05	1	<u>Tank</u>	
		For remilled maize.	
		Volume	Approx. 1.5 M <sup>3</sup>
		Material	Stainless steel 316
4.06	1	<u>Rotary Valve with speed control</u>	
		Capacity	Approx. 12 MT/h
		Material	Stainless steel 316

4.07	1	<u>Fibre mill</u> To release starch/gluten particles from maize fibres.	500	MT/Day	maize
		Capacity	equivalent		
		Material	Stainless steel 316		
4.08	1	<u>Tank</u> For Fibre washing			
		Volume	Approx. 3 M <sup>3</sup>		
		Material	FRP		
4.09	1	<u>Agitator</u>			
		Material	Stainless Steel 316		
4.10	1	<u>Centrifugal Pump</u> To pump the suspension to the fibre washing station.			
		Capacity	Approx. 20 M <sup>3</sup> /h		
		Delivery head	Approx. 20 M		
		Material	Stainless steel 316		
4.11	7	<u>Fibre washing screens</u> For counter current washing of maize fibre.	500	MT/Day	maize
		Capacity	equivalent.		
		Material	Stainless Steel 316		
4.12	1	<u>Multi-compartment cascade tank</u> For counter current washing of maize fibre			
		Total volume	Approx. 7 M <sup>3</sup>		
		Material	Stainless Steel 316		
4.13	7	<u>Centrifugal Pumps</u> To pump maize fibre slurry through the fibre washing system.			
		Capacity	Approx. 30 M <sup>3</sup> /h		
		Delivery head	Approx. 30 M		
		Material	Stainless steel 316		



## 5. Starch Separations And Refining

5.01	1	<u>Tank</u>	
		To collect starch/glutenSlurry	
		Volume	Approx. 15 M <sup>3</sup>
		Material	FRP
5.02	1	<u>Agitator</u>	
		To mix starch/gluten slurry, all parts coming into contact with the product to be made from stainless steel AISI 316, complete with gear motor and all accessories required.	
		Material	Stainless Steel 316
5.03	1	<u>Centrifugal Pump</u>	
		To pump starch/gluten slurry to the Primary separator.	
		Capacity	Approx. 30 M <sup>3</sup> /h
		Delivery head	Approx. 60 M
		Material	Stainless steel 316
5.04		<u>Heat Exchanger for Starch Milk suitable</u>	
		for cooling starch milk from 36 to 30 deg. C	
		Type	Plate type.
		Material	Stainless steel 316
5.05	3	<u>Degritting cyclones - two stage</u>	
	1	Rotary Strainer	
		Material	Stainless steel 316/Ceramic.

5.06	1	<u>Wash Water Tank</u>	
		Capacity	Approx. 3 M <sup>3</sup>
		Material	FRP
5.07	1	<u>Centrifugal Pump</u>	
		To supply wash water to the separator.	
		Capacity	Approx. 10 M <sup>3</sup> /h
		Delivery head	Approx. 20 M
5.08	1	<u>Tank</u>	
		Material Stainless steel 316	
		For partly refined starch milk.	
		Volume	Approx. 7.5 M <sup>3</sup>
		Material	FRP
5.09	1	<u>Agitator</u>	
		For partly refined starch milk.	
5.10	1	<u>Centrifugal Pump</u>	
		Material Stainless Steel 316	
		To pump starch slurry to the hydrocyclone unit.	
		Capacity	Approx. 15 M <sup>3</sup> /h
		Delivery head	Approx. 30 M
5.11	1	<u>Rotary Strainer</u>	
		Material Stainless steel 316	
		To filter out particles that could block hydrocyclonettes.	
		Capacity	Approx. 15 M <sup>3</sup> /h
5.12	1	<u>Tank</u>	
		Material Stainless steel 316	
		For wash water	
		Volume	Approx. 5 M <sup>3</sup>
		Material	FRP

5.13	1	<u>Centrifugal Pump</u>	
		For wash water.	
		Capacity	Approx. 10 M <sup>3</sup> /h
		Delivery head	Approx. 60 MLC
		Material	Stainless steel 316
5.14	1	<u>Heat Exchanger</u>	
		for heating wash water to 50 deg.	
		C	
		Type	Plate heat exchanger.

		Capacity	Approx. 10 M <sup>3</sup>
		Material	Stainless steel 316
5.15	1	<u>Tank</u>	
		For safety water	
		Volume	Approx. 15 M <sup>3</sup>
		Material	FRP
5.16	1	<u>Tank</u>	
		To hold caustic solution for cleaning purpose with steam sparger.	
		Volume	Approx. 5 M <sup>3</sup>
		Material	Stainless Steel 316
5.17	1	<u>Centrifugal Pump</u>	
		To supply caustic water to the refining separator.	
		Capacity	Approx. 40 M <sup>3</sup> /h
		Delivery head	Approx. 30 M
		Material	Stainless steel 316

## 6. Gluten Concentration

6.01	2	<u>Gluten Foam Boxes suitable for 500 TPD Equivalent corn.</u>	
		Volume	1 M <sup>3</sup>
		Material	Stainless steel 316
6.02	1	<u>Tank</u>	
		To hold gluten water.	
		Volume	Approx. 25 M <sup>3</sup>
		Material	FRP
6.03	1	<u>Agitator</u>	
		For gluten water tank	
		Material	Stainless steel 316
6.04	1	<u>Centrifugal Pump</u>	
		To supply gluten water to the separator.	
		Capacity	Approx. 25 M <sup>3</sup> /h
		Delivery head	Approx. 20 M
		Material	Stainless steel 316
6.05	1	<u>Rotary Stainer</u>	
		For gluten water.	
		Capacity	25 M <sup>3</sup> /H
		Material	Stainless steel 316
6.07	2	<u>Tank for Gluten Concentrates</u>	
		To hold gluten water.	
		Capacity	Approx. 7.5 M <sup>3</sup>
		Material	FRP
6.08	2	<u>Agitators</u>	
		For Gluten concentrate tank.	
		Material	Stainless steel 316
6.09	1	<u>Centrifugal Pump</u>	
		To recycle gluten concentrate.	
		Capacity	Approx. 10 M <sup>3</sup> /h
		Delivery head	Approx. 15 M
		Material	Stainless steel 316



6.10	1	Centrifugal Pump To pump gluten concentrate to the rotary vacuum drum filter.		
		Capacity	Approx.	7.5 M <sup>3</sup> /h
		Delivery head	Approx.	20 M
		Material		Stainless steel 316
6.11	2	Process Water tanks		
		Capacity	Approx.	15 M <sup>3</sup> /h
		Material		FRP
6.12	2	Process water pumps		
		Capacity	Approx.	20 M <sup>3</sup> /h
		Delivery head	Approx.	30 M
		Material		Stainless steel 316
6.13	1	Filter presses For gluten dewatering suitable for 500 TPD Maize equivalent with all accessories.		
6.14		Screw Conveyor For conveying gluten cake to dryer.		
		Capacity	500 MT/Day	maize equivalent.
		Material		Stainless steel 304
		Sealing	water	
6.15	1	recirculation System for vacuum pump of Rotary filter.		
		Material		Stainless steel 316/MS
6.16	1	Tank for steam condensate.		
		Volume		3 M <sup>3</sup>
		Material		Stainless steel 316
6.17	1	Centrifugal Pump For steam condensate		
		Capacity	Approx.	5 M <sup>3</sup> /h
		Delivery head	Approx.	20 MLC
		Material		Stainless steel 316

## **7. Germ dewatering and drying**

- 7.01 1 Screw press  
To dewater maize germ.  
Capacity Approx. 500 T/24 h maize equivalent  
All product contact parts to be SS 316  
dewatering screw inside conical screen, driven  
by an electric motor via a gear box, all mounted  
on a M S frame, complete with all accessories  
required.
- 7.02 1 Germ Dryer  
To dry dewatered maize germ  
Capacity Approx.. 250 Kg/h Water evaporation.  
Carbon steel tube bundle, with SS 316 lifter  
blades driven by an electric motor via a gear  
box, carbon steel housing with wet product  
contact parts in SS 316, steam heater for purge  
air, rotary steam and condensate joints,  
complete with all accessories required,  
including a vapour extraction fan with ductwork  
made of SS 304 and electric motor,  
a rotary valve with geared motor for product  
discharge.

## 8. Steeping Water Concentration

- 8.01 1 Tank  
To collect light steep liquor from the steeping tanks.  
Volume Approx. 40 M<sup>3</sup>  
Material Stainless steel 316  
Complete with inlet and outlet connections and all accessories required
- 8.02 1 Centrifugal Pump  
To pump the light steep liquor to the evaporator..  
Volume Approx. 7.5 M<sup>3</sup> / h  
Delivery Head Approx. 20 M.
- 8.03 1 Duplex Strainer.  
To remove the extraneous particles from the light steep liquor.  
Capacity. Approx. 10 M<sup>3</sup> / h  
All product contact parts to be of SS 316, complete with mesh screens, 3-way change-over valves, inlet and outlet connections, and all accessories required.

- 8.04 1 Multiple effect evaporator with thermal vapour recompression  
 To concentrate light steep water  
 Capacity. Approx. 4750 Kg/ h  
 water evaporation.  
 Complete package unit to  
 include:  
 feed balance tank, 500 Lit.  
 capacity.  
 Centrifugal pumps for product and condensate.  
 Heat Exchangers for preheating the product.  
 Surface condenser for vapour.  
 Falling film evaporators with product vapour  
 separator.  
 Thermal vapour compressor.  
 Watering- ring type vacuum  
 pump.  
 Valves and  
 instruments  
 for automatic plant control.,  
 Interconnecting pipe work and  
 ducts,  
 and all accessories required,  
 all product contact parts are made of SS 316.
- 8.05 1 Tank  
 To collect Conc.  
 Steep liquor from the evaporator  
 Volume Approx. 3 M<sup>3</sup>  
 Material SS 316  
 Jacket for steam  
 heating SS 316
- 8.06 1 Agitator.  
 To mix concentrated steep liquor,  
 all product contact parts to be of SS 316,  
 complete with geared motor and all accessories  
 required .
- 8.07 1 Displacement pump  
 To pump concentrated steep liquor  
 to  
 animal feed dryer.  
 Capacity. Approx. 2 M<sup>3</sup> / h  
 Delivery head Approx. 60 M  
 Parts coming in contact with the product to be of  
 stainless steel and EPDM

## Section: 9.00

- 9.01 1 Gluten Flash Dryer.  
For drying gluten cake after filter presses.  
System complete with direct fired hot air generator with burner assembly, LDO tank, feed conveyor, swing fan, recycle conveyor, flash duct, cyclones, exhaust fan and rotary valve below cyclones.  
All product contact parts to be in SS 316.

## 10.00 :Animal Feed Dewatering And Drying

- 10.01 1 Screw Press  
To dewater maize fibre.
- |          |   |
|----------|---|
| Capacity | Approx. 500<br>T/Day<br>Maize grind<br>equivalent.<br>Stainless |
| Material | steel 316   |
- 10.02 1 Feed conditioner  
For intensive mixing of recycled dried feed, concentrated mixed liquor with thick phase slops and dewatered maize fibre.
- |          |               |
|----------|---------------|
| Capacity | Approx. 3 T/h |
|----------|---------------|



## 11. Starch Dewatering and Drying

- 11.01 1 Tank for Feeding Centrifuge For starch milk  
Volume Approx 2 M<sup>3</sup>  
Material Stainless Steel 316
- 11.02 2 Peeler Centrifuge  
For dewatering starch milk  
Capacity Approx. 60 T/24 h

Parts coming into contact with the product are made from stainless steel SS 304 complete with perforated basket, housing, disc brake, peeling knife, discharge screw conveyor with gear motor-belt drive and hydraulic coupling for main motor, protection device, hydraulic system with oil pump, 2 special valves for filling the centrifuge with starch milk, electric control panel for automatic operation, special tools and all required accessories.

- 11.03 1 Screw Conveyor.  
For conveying dewatered starch cake to starch dryer  
Capacity Approx. 4.0 MT/ h  
Material Stainless steel 304.

- 11.04 1 Starch Dryer  
Designed as pneumatic flash dryer.  
Capacity Approx. 96 T/24 h  
commercial starch.  
Material Stainless steel AISI 316  
in welded construction, complete with steam Air heater  
dryer ventilator, special rotating feeding device, drying duct,  
battery of cyclone, reception bunker , rotary valve,  
all required electrical gear motors, inlet and outlet chutes and  
fittings and all required accessories.



11.05	1	<u>Starch Sifter</u> of tumbling type with two decks for separating starch grits. Capacity	Approx. 4000 Kg/ h commercial starch.
		Material	Stainless steel AISI 316
11.06	1	Buffer Tank with ventilator  For sifted starch. Volume	Approx. 1 M3
		Material	Stainless Steel 316
11.07	1	Tank  For dissolving starch grits. Volume	Approx. 2 M <sup>3</sup>
		Material	FRP
11.08	1	Agitator  for dissolving starch grits. Material	Stainless steel 316
11.09	1	Centrifugal Pump  For conveying Capacity	dissolved starch milk. Approx. 3.2 M <sup>3</sup> /h
		Delivery head	Approx. 15 M
		Material	Stainless steel 316





## 12. Sorbitol and maltodextrin manufacturing section

- 12.01 2 Tank for Feeding Centrifuge For starch milk  
Volume Approx 1.5 M<sup>3</sup>  
Material Stainless Steel 316
- 12.02 3 Screw Conveyor.  
For conveying dewatered starch cake to starch dryer  
Capacity Approx. 3.0 MT/ h  
Material Stainless steel 304.
- 12.03 1 Drying unit  
Designed as pneumatic flash dryer.  
Capacity Approx. 80 T/24 h commercial starch.  
Material Stainless steel AISI 316
- 12.04 1 Starch Sifter  
of tumbling type with two decks for separating starch grits.  
Capacity Approx. 2000 Kg/ h commercial starch.  
Material Stainless steel AISI 316
- 12.05 1 Tank  
For dissolving starch grits.  
Volume Approx. 2 M<sup>3</sup>  
Material FRP



## 13. DMH section

13.01	1	<u>Tank</u>	
		To collect starch/glutenSlurry	
		Volume	Approx. 15 M <sup>3</sup>
		Material	FRP
13.02	1	<u>Agitator</u>	
		To mix starch/gluten slurry, all parts coming into contact with the product to be made from stainless steel AISI 316, complete with gear motor and all accessories required.	
13.03	1	<u>Centrifugal Pump</u>	Material Stainless Steel 316
		To pump starch/gluten slurry to the Primary separator.	
		Capacity	Approx. 30 M <sup>3</sup> /h
		Delivery head	Approx. 60 M
13.04	1	<u>Heat Exchanger for Starch Milk suitable</u>	Material Stainless steel 316
		for cooling starch milk from 36 to 30 deg. C	
		Type	Plate type.
13.05	2	<u>Degritting cyclones - two stage</u>	Material Stainless steel 316
	1	Rotary Strainer	
		Material	Stainless steel 316/Ceramic.



13.06	1	Drying unit	
		Designed as pneumatic flash dryer.	
		Capacity	Approx. 85 T/24 h commercial starch.
		Material	Stainless steel AISI 316
13.07	1	<u>Tank</u>	
		For wash water	
		Volume	Approx. 5 M <sup>3</sup>
		Material	FRP

A = Approximate. Cost of the maize processing machinery and equipments

**Total Cost      Rs.80,00,00,000.00**



## **B. HANDLING/HOLDING & STORAGE EQUIPMENTS**

1. M.S Storage Silo  
Cap: 50 tons 15 No. Rs. 1,25,00,000.00
2. Vibro-screen (Automatic) with 25 HP  
motor and accessories  
Cap: 30-50 tons/hour 2 No. Rs. 1,80,00,000.00
3. Automatic weighing, filling, & bags  
sealing machine 1 No. Rs. 1,50,00,000.00
4. Pipes, pumps, motors Airlock,  
structures & others Rs. 90,00,000.00
5. Electrical fittings, switchgear,  
MCB, cables, & others Rs. 50,00,000.00

### **B = Approximate. Cost of the HANDLING/HOLDING & STORAGE EQUIPMENTS**

**Total Cost Rs. 5,95,00,000.00**

## **Lab testing equipment**

Sr.No.	Chemical Testing/ Particulars	Quantity
1	Refractometer	1
2	TDS meter	1
3	PH meter	1
4	Water Distillation Unit	1
5	Laboratory Oven with Air Circulation	1
6	Scientific Balance	1
7	Heating menthal	1
8	Muffle Furnace	1
9	Electric Heating Plate	1
10	Thermometer	1
11	Bursting Strength Tester	1
12	Water Bath	1
	(Microbiological Testing)	
1	Rotary Shakers	1
2	Airflow Oven Drier	1
3	Laminar Airflow cabinet	1



4	Centrifuge Machine	1
5	Microscope	1
6	Autoclave	1
7	Refrigerator	1
8	Spirit Lamp	1
9	Incubator	1
10	Colony counter	1
11	Balance (chemical)	1 Lot
Sr.No.	List of lab Glass Ware	Quantity
1	Round Bottom Flask	
2	Beakers	
3	Volumetric Flask	
4	Conical Flask	
5	Pipette Stand	
6	Measuring Cylinder	
7	Burette	
8	Pipette	
9	Glass Funnel	
10	Clamps & Stand	
11	Pipetter(suction for pipette)	
12	Silica beads	
13	Sampling Probe	
14	Burette Stand With Clamp	
15	Tripod Stand	
16	Funnel	
17	Petri Plate	
18	Silica Crucible	
19	Glass beads	
20	Protein Estimation unit	
27	Fat Extraction Unit	
31	Spirit Lamp	
32	Reagent Bottles	
33	Glass Rod	
34	Ashless Filter Paper	
35	Normal Filter Paper	
36	Bottle Brush	
37	S.S. Scissor	
38	Rubber Corks	
39	Cappillary Tubes	



# ENGINEERS INDIA RESEARCH INSTITUTE

*We Create Industrialists*

40	Cork Borer	
41	Rubber Pipes	
42	Triple Stand	

C = Approximate. Cost of the lab equipments Total Cost Rs. 75,00,000.00

### ***Total cost of machinery and equipments***

Grand Total A+B+C = Rs. 80,00,00,000.00+ Rs. 5,95,00,000.00+ Rs.75,00,000.00

**= Rs. 86,70,00,000.00**

-----  
TOTAL    Rs. 86,70,00,000.00  
-----



## PLANT ECONOMICS

Rated Plant capacity	=	MAIZE PROCESSING PLANT
		1. Starch 60,000 MT
		2. Liquid Glucose 8,000 MT
		3. Dextrose Monohydrate 2,500 MT
		4. Maize Germ 200 MT
		5. Sorbitol 4,000 MT
		6. Dextrin 3,000 MT
		7. Gluten 2,500 MT
		8. Animal feed, 8,000 MT

### Basis

No. of working days	=	25 days/month
	=	300 days/annum
No. of shifts	=	3 per day
One shift	=	8 hours

Currency - Rs.



## LAND & BUILDING

1. Land 30 Acre @ Rs. 40,00,000/-per acre	Rs.	12,00,00,000.00
2. Site Development charges	Rs.	40,00,000.00
3. Civil Construction & Building:Maize receiving godown 5000 sq.mtr @ Rs. 7500/-	Rs.	3,75,00,000.00
4. Maize/Corn storage Silos 1000 Sq.mtr @ Rs. 7500/-per sq.mtrs.	Rs.	75,00,000.00
5. Maize Steeping section 2500 sq.mtr @ Rs. 7500/-per sq.mtrs.	Rs.	1,87,50,000.00
6. Wet Milling Section 2000 sq.mtrs. @ Rs. 7500/-sq.mtrs.	Rs.	1,50,00,000.00
7. Germ Drier and Oil separation area 1000 sq.mtrs.@ Rs. 7500/-per sq.mtr	Rs.	75,00,000.00
8. Cattle feed drier area 2000 sq.mtr @ Rs. 7500/-sq.mtrs	Rs.	1,50,00,000.00
9. Starch drier & Packing area 1000 sq.mtrs. @ Rs. 7500/-per sq.mtrs.	Rs.	75,00,000.00
10. Dextrin/Sorbitol processing area 1000 sq.mtrs.@ Rs. 7500/-per sq.mtr	Rs.	75,00,000.00
11. Raw Material Storage area 1000 sq.mtrs. @ Rs. 7500/-	Rs.	75,00,000.00
12. Packaging material storage 800 sq.mtrs. @ Rs. 7500/-per sq.mtrs.	Rs.	60,00,000.00
13. Cattle feed storage 2000 sq.mtrs. @ Rs. 7500/-per sq.mtrs.	Rs.	1,50,00,000.00
14. Glucose Dextrose Plants 1500 sq.mtr @ Rs.7500/-per sq.mtrs.	Rs.	1,12,50,000.00
15. Provision for future expansion 3000 sq.mtrs.@ Rs. 500/-per sq.mtrs	Rs.	15,00,000.00





# ENGINEERS INDIA RESEARCH INSTITUTE

*We Create Industrialists*

16. Boiler House 200 sq.mtrs. @ Rs. 6500/-per sq.mtrs.	Rs.	13,00,000.00
17. Water treatment & services area 100 sq.mtrs. @ Rs. 6500/-	Rs.	6,50,000.00
18. Work shop 300 sq.mtrs.@ Rs. 6500/- per sq.mtrs.	Rs.	19,50,000.00
19. Sulpher dioxide plant area 1000 sq.mtrs. @ Rs. 6500/-per sq.mtrs.	Rs.	65,00,000.00
20. Electrical substation 500 sq.mtrs @ Rs. 6500/-per sq.mtrs.	Rs.	32,50,000.00
21. First aid Post 300 sq.mtrs. @ Rs. 6500/- per sq.mtrs.	Rs.	19,50,000.00
22. Security Office 200 sq.mtrs. @ Rs. 6500/-per sq.mtrs.	Rs.	13,00,000.00
23. Time Office 100 sq.mtr @ Rs. 6500/- per sq.mtrs.	Rs.	6,50,000.00
24. Truck Scale Weight bridge 500 sq.mt @ Rs. 6500/-per sq.mtrs.	Rs.	32,50,000.00
25. Canteen 400 sq.mtrs. @ Rs. 6500/- per sq.mtrs.	Rs.	26,00,000.00
26. Administrative office 500 sq.mtrs. @ Rs. 10000/-per sq.mtrs.	Rs.	50,00,000.00
27. Laboratory cum R & D center 500 sq.mtrs. @ Rs. 8000/-per sq.mtrs.	Rs.	40,00,000.00
		-----
	<b>TOTAL</b>	<b>Rs. 31,39,00,000.00</b>
		-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 4

## PLANT & MACHINERY

(1.) Approximate. Cost of the Maize Processing Machinery and Equipment		Rs.	80,00,00,000.00
(2.) Handling/Holding & Storage Equipments:-			
1. M.S. Storage Silo Cap: 50 Tons.	15 No.	Rs.	1,25,00,000.00
2. Vibro-Screen (Automatic) with 25 HP Motor and Accessories Cap: 30-50 Tons/hour	2 No.	Rs.	1,80,00,000.00
3. Automatic Weighing, Filling & Bags Sealing Machine	1 No.	Rs.	1,50,00,000.00
4. Pipes, Pumps, Motors Airlock, Structures & others		Rs.	90,00,000.00
5. Electrical Fittings, Switchgear, MCB, Cables & others		Rs.	50,00,000.00
(3.) Approximate. Cost of the Lab Equipments Total Cost		Rs.	75,00,000.00
			-----
	<b>TOTAL</b>	Rs.	<b>86,70,00,000.00</b>
			-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 5

OTHER FIXED ASSETS

1. Water Electricity connection	Rs.	12,50,000.00
2. Site fabrication work	Rs.	15,00,000.00
3. Erection & Commissioning	Rs.	25,00,000.00
4. Preliminary & Preoperative expenses	Rs.	20,00,000.00
5. Office Furniture and equipment	Rs.	20,00,000.00
6. DG Generator with accessories	Rs.	1,20,00,000.00
		-----
TOTAL	Rs.	2,12,50,000.00
		-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 6

**FIXED CAPITAL**

1. LAND & BUILDING	Rs.	31,39,00,000.00
2. PLANT & MACHINERY	Rs.	86,70,00,000.00
3. OTHER FIXED ASSETS	Rs.	2,12,50,000.00
		-----
<b>TOTAL</b>	<b>Rs.</b>	<b>1,20,21,50,000.00</b>
		-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 7

## WORKING CAPITAL REQUIREMENT/MONTH

### RAW MATERIALS

1. Maize 12,500 MT @ Rs. 16,000/-per MT	Rs.	20,00,00,000.00
2. Sulphur 9.5 MT @ Rs. 45000/-per MT	Rs.	4,27,500.00
3. Sulphuric acid 50 MT @ Rs. 8000/-per MT	Rs.	4,00,000.00
4. Caustic soda 50 MT @ Rs. 28000/-per MT	Rs.	14,00,000.00
5. Activated Carbon 5 MT @ Rs. 35000/-per MT	Rs.	1,75,000.00
6. Soda Ash 25 MT @ Rs. 12500/-Per MT	Rs.	3,12,500.00
7. Bone Black 8 MT @ Rs. 35000/-per MT	Rs.	2,80,000.00
8. Lubricating Oils 1.8 MT	Rs.	1,17,000.00
9. Fuel Oil 10000 Ltr. @ Rs. 60/-Ltr	Rs.	6,00,000.00
<b>TOTAL</b>	Rs.	<b>20,37,12,000.00</b>



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 8

SALARY & WAGES / MONTH

1. Managing Director	1 No.	Rs.	80,000.00
2. Secretary	1 No.	Rs.	25,000.00
3. Works Manager	1 No.	Rs.	50,000.00
4. Accounts & Admn. Officer	1 No.	Rs.	25,000.00
5. Chief Chemical Engineer	1 No.	Rs.	40,000.00
6. Production & Maintenance superintendent	1 No.	Rs.	25,000.00
7. Purchase Officer	1 No.	Rs.	30,000.00
8. Sales Officers	4 No.	Rs.	60,000.00
9. Asst. Admn. Officer	1 No.	Rs.	20,000.00
10. Junior Chemical Engineers	3 No.	Rs.	60,000.00
11. Chemists	3 No.	Rs.	75,000.00
12. Mechanical Engineer	1 No.	Rs.	25,000.00
13. Electrical Engineer	1 No.	Rs.	18,000.00
14. Watch & Ward Officer	1 No.	Rs.	8,000.00
15. Manager quality control	2 No.	Rs.	60,000.00
16. Laboratory Assistant	2 No.	Rs.	24,000.00
17. Supervisors	4 No.	Rs.	60,000.00
18. Store Keepers	2 No.	Rs.	20,000.00
19. Sales Assistants	2 No.	Rs.	24,000.00
20. Stenographers	10 No.	Rs.	1,00,000.00
21. Clerk-cum-typists	2 No.	Rs.	17,000.00
22. Operators	25 No.	Rs.	2,12,500.00



23. Skilled workers	24 No.	Rs.	2,88,000.00
24. Unskilled workers	30 No.	Rs.	2,25,000.00
25. Boiler Atendants	3 No.	Rs.	30,000.00
26. Pump House Men	3 No.	Rs.	30,000.00
27. Compressor Room Men	3 No.	Rs.	30,000.00
28. Packers	4 No.	Rs.	34,000.00
29. Driers	5 No.	Rs.	45,000.00
30. Watchmen	4 No.	Rs.	32,000.00
31. Peons	4 No.	Rs.	30,000.00
32. Sweepers	4 No.	Rs.	30,000.00
33. Helpers	10 No.	Rs.	80,000.00
	<b>TOTAL</b>	Rs.	19,12,500.00
			-----
Plus perks @ 33% p.a.		Rs.	6,31,125.00
	<b>TOTAL</b>	Rs.	25,43,625.00
			-----



MAIZE PROCESSING PLANT ETC....(EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 9

## UTILITIES AND OVERHEADS

1. Power Consumption of 408000 Kwatt hrs @ Rs. 7.00 per Kwatt hr.	Rs.	28,56,000.00
2. Water Consumption of 65000 KLs @ Rs. 4.00 per KL	Rs.	2,60,000.00
3. Fuel Oil 15 MT @ Rs. 60/-per Ltr	Rs.	9,00,000.00
4. Transportation	Rs.	15,00,000.00
5. Packaging material @ Rs. 22,50,000 P.M.	Rs.	22,50,000.00
6. Sales Promotion and Advertising	Rs.	15,00,000.00
7. Administrative Expenses	Rs.	5,00,000.00
	-----	
	TOTAL	Rs. 97,66,000.00
		-----

Total load is 748 Kwatts





MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 10

### TOTAL WORKING CAPITAL/MONTH

1. RAW MATERIAL	Rs.	20,37,12,000.00
2. SALARY & WAGES	Rs.	25,43,625.00
3. UTILITIES & OVERHEADS	Rs.	97,66,000.00
		-----
	TOTAL	Rs. 21,60,21,625.00
		-----

1. WORKING CAPITAL FOR 3 MONTHS	Rs.	64,80,64,875.00
2. MARGIN MONEY FOR W/C LOAN	Rs.	16,20,16,218.75

### COST OF PROJECT

TOTAL FIXED CAPITAL	Rs.	1,20,21,50,000.00
MARGIN MONEY	Rs.	16,20,16,218.75
		-----
	TOTAL	Rs. 1,36,41,66,218.75
		-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 11

**TOTAL CAPITAL INVESTMENT**

TOTAL FIXED CAPITAL	Rs. 1,20,21,50,000.00
TOTAL WORKING CAPITAL FOR 3 MONTHS	Rs. 64,80,64,875.00
	-----
<b>TOTAL</b>	<b>Rs. 1,85,02,14,875.00</b>
	-----



MAIZE PROCESSING PLANT ETC.... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 12

## COST OF PRODUCTION/ANNUM

1. Working Capital for 1 year	Rs.2,59,22,59,500.00
2. Interest @ 13.50% on T.C.I	Rs.24,97,79,008.13
3. Depreciation @ 10.00% on buildings	Rs. 1,93,90,000.00
4. Depreciation @ 20.00% on Plant and Machinery	Rs.17,34,00,000.00
	-----
TOTAL	Rs.3,03,48,28,508.13
	-----



MAIZE PROCESSING PLANT ETC... (EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 13

TURN OVER/ANNUM

1. Starch 60,000 MT @ Rs.28,000/- per MT.	Rs.1,68,00,00,000.00
2. Liquid Glucose 8,000 MT @ Rs. 60,000/-MT	Rs.48,00,00,000.00
3. Dextrose Monohydrate 2,500 MT @ Rs. 1,50,000/-MT	Rs.37,50,00,000.00
4. Maize Germ 200 MT @ Rs. 58,300/-Per MT	Rs. 1,16,60,000.00
5. Sorbitol 4,000 MT @ Rs. 1,80,000/-Per MT	Rs.72,00,00,000.00
6. Dextrin 3,000 MT @ Rs. 1,80,000/-per MT	Rs.54,00,00,000.00
7. Gluten 2,500 MT @ Rs. 90,000/-per MT	Rs.22,50,00,000.00
8. Animal feed, 8,000 MT @ Rs. 22,000/-per MT	Rs.17,60,00,000.00
<b>TOTAL</b>	----- <b>Rs.4,20,76,60,000.00</b> -----



# ENGINEERS INDIA RESEARCH INSTITUTE

*We Create Industrialists*

$$\begin{aligned}\text{PROFIT} &= \text{RECEIPTS} - \text{COST OF PRODUCTION} \\ &= 4,20,76,60,000.00 - 3,03,48,28,508.13 \\ &= 1,17,28,31,491.88\end{aligned}$$

$$\begin{aligned}\text{PROFIT SALES RATIO} &= \text{Profit} / \text{Sales} \times 100 \\ &= \frac{1,17,28,31,491.88}{4,20,76,60,000.00} \times 100 \\ &= 27.87 \%\end{aligned}$$

$$\begin{aligned}\text{RATE OF RETURN} &= \text{Operating profit} / \text{T.C.I} \times 100 \\ &= \frac{1,17,28,31,491.88}{1,85,02,14,875.00} \times 100 \\ &= 63.39 \%\end{aligned}$$



BREAK EVEN POINT (B.E.P)

Fixed Costs of the plant are as under -

1. Interests	Rs.24,97,79,008.13
2. Depreciation	Rs.19,27,90,000.00
3. 40.00% of salaries	Rs. 1,22,09,400.00
4. 40.00% of overheads	Rs. 4,68,76,800.00
	-----
TOTAL	Rs.50,16,55,208.13
	-----

$$\begin{aligned} \text{B.E.P.} &= \frac{\text{FIXED COSTS}}{\text{FIXED COSTS} + \text{PROFIT}} \times 100 \\ &= \frac{50,16,55,208.13}{50,16,55,208.13 + 1,17,28,31,491.88} \times 100 \\ &= 29.96 \% \end{aligned}$$

LAND MAN RATIO = Total land / Manpower

$$30 : 164 :: 0 : 1$$



MAIZE PROCESSING PLANT ETC....(EIRI/DFR/1280) J.C. 9941  
J.C. 9941

Page A- 15

## RESOURCES FOR FINANCE

1. Term loans from Financial institutions  
( 65.00 % of fixed capital )  
at @13.50% p.a rate of interest                      Rs. 78,13,97,500.00
  
2. Bank loans for 3 months  
( 65.00 % of working capital )  
at @ 13.50% p.a rate of interest                      Rs. 42,12,42,168.75
  
3. Self raised capital from even  
funds & loans from close ones to  
meet the margin money needs at a  
@ 13.50% p.a rate of interest                      Rs. 64,75,75,206.25

-----  
TOTAL Rs. 1,85,02,14,875.00  
-----



We hope **Detailed Feasibility Report** in your possession at the time, must have conveyed you the elementary idea on process data, market and economics. We feel you must have now taken a decision to finalize your project plan for ultimate implementation in a successful manner. Before you go ahead, we suggest you to take our **MARKET SURVEY CUM DETAILED TECHNO ECONOMIC FEASIBILITY REPORT**.

"EIRI" offer you **MARKET SURVEY CUM DETAILED TECHNO ECONOMIC FEASIBILITY REPORT** on this project.

**Brief contents of MARKET SURVEY CUM DETAILED TECHNO ECONOMIC FEASIBILITY REPORT** are as under :

- Introduction
- Properties
- BIS (Bureau of Indian Standard) Specifications & Requirements
- Uses & Applications
- Present Indian Market Position
- Expected Future Demand
- Export & Import Statistics Data
- Names and Addresses of Existing Units (Present Manufactures)
- List of Plant & Machineries
- Miscellaneous Items and Accessories
- Instruments, Laboratory Equipments and Accessories
- Electrification, Electric Load and Water
- Maintenance, Suppliers/Manufacturers of Plant and Machineries
- Process of Manufacture with formulae if applicable
- Flow Sheet Diagram
- List of Raw Materials
- Availability of Raw Materials
- Requirement of Staff & Labour
- Personnel Management
- Skilled & Unskilled Labour
- Requirement of Land Area
- Built up Area
- Plant Layout.

**along with financial details as under:**

Summary of Capital Cost of Project  
Land & Side Development Exp.  
Buildings  
Plant & Machineries  
Misc. Fixed Assets  
Technical Know how Fees & Exp.  
Preliminary Expenses  
Pre-operative Expenses  
Provision for Contingencies

below mentioned financial statements (Annexure) will be for 5 to 10 Years

- Annexure :: Cost of Project and Means of Finance
- Annexure :: Output, Profitability and Cash Flow Chart
- Annexure :: Assessment of Working Capital requirements





# ENGINEERS INDIA RESEARCH INSTITUTE

*We Create Industrialists*

Annexure ::	Sources of Finance
Annexure ::	Balance Sheets
Annexure ::	Break-Even Analysis and profitability analysis.
Annexure ::	Quantitative Details-Output/Sales/Stocks
Annexure ::	Sales Realisation
Annexure ::	Raw Material Cost
Annexure ::	Other Raw Material Cost
Annexure ::	Packing Material Cost
Annexure ::	Consumables, Store etc.,
Annexure ::	Employees Expenses
Annexure ::	Fuel Expenses
Annexure ::	Power/Electricity Expenses
Annexure ::	Repairs & Maintenance Exp.
Annexure ::	Other Mfg. Expenses
Annexure ::	Administration Expenses
Annexure ::	Selling Expenses
Annexure ::	Depreciation Charges - Profitability
Annexure ::	Depreciation Charges
Annexure ::	Interest and Repayment - Term Loans
Annexure ::	Tax on Profit
Annexure ::	Assumptions for Profitability workings
Annexure ::	Assessment of Working Capital

**Engineers India Research Institute (EIRI) is a renowned name in the industrial world for offering technical and financial consultancy services.**

**EIRI services are:**

Detailed Feasibility Reports  
New Project Identification  
Project Feasibility and Market Study  
Identification of Lucrative Industrial Project Opportunities  
Preparation of Project Profiles / Pre-Investment and Detailed Feasibility Studies,  
Market Surveys / Studies, Market Survey Cum Detailed Techno-Economic Feasibility Reports  
Project Reports in CD Roms  
Identification of Plant /Process/Machinery and Equipment, Industrial General Guidance for setting up new industrial projects.

**Price Rs. 20,000/- (Rs. Twenty Thousand only) or US\$ 400/- (US Dollars Four Hundred Only) for MARKET SURVEY CUM DETAILED TECHNO ECONOMIC FEASIBILITY REPORT.**

**PLEASE SEND YOUR CONFIRMED ORDER AT:**

**ENGINEERS INDIA RESEARCH INSTITUTE**

**4449, Nai Sarak, Main Road, Delhi-110 006 (India)**

**Ph: 91-11-23916431, 23918117, 45120361, 64727385, 23947058**

**E-Mail: [eiribooks@yahoo.com](mailto:eiribooks@yahoo.com), [eiriprojects@gmail.com](mailto:eiriprojects@gmail.com)**

**Website: [www.eiriindia.org](http://www.eiriindia.org), [www.eiribooksandprojectreports.com](http://www.eiribooksandprojectreports.com)**

**Mob: 9811437895, 9811151047**